AMENDMENT(S) TO THE SPECIFICATION

Please replace the paragraph beginning at page 7, line 9, with the following rewritten paragraph:

The plant represented in Fig. 1 has four fluidized-bed reactors, 1 to 4, subsequently connected in series, wherein iron-oxide-containing ore, such as fine ore, via an ore feed duct 5 is fed to the first fluidized-bed reactor 1, in which heating up to a predetermined temperature takes place, as will be explained in more detail in the following. Subsequently, the fine ore, f.i. having a chemical composition according to the following table, is [[conduced]] conducted from fluidized-bed reactor to fluidized-bed reactor via the feed ducts 6, with fluidized-bed zones forming within each fluidized-bed reactor 1 to 4. The completely reduced material (sponge iron) is hot-briquetted in a briquetting means 7. If necessary, the reduced iron is protected from reoxidation during briquetting by an inert-gas system that is not represented.

Chemical analysis of the fine ore (percent by weight)									
Fetot	Fe_2O_3	FeO	CaO	SiO_2	Al_2O_3	MgO	TiO_2	C	LOI
67.8	96.9	0.06	0.06	1.38	0.6	0.04	0.04	0.01	0.95

Please replace the paragraph beginning at page 7, line 27, with the following rewritten paragraph:

Production of the reducing gas is done by reforming natural gas, supplied via duct 11 and desulfurized in a desulfurization plant 12, in a reformer 10. The gas formed from natural gas and vapour and leaving the reformer 10 substantially consists of H_2, CO, CH_2, H_2O and CO_2. Via the reformed gas duct 13, this reformed natural gas is fed to one or several heat exchangers 14, in which it is cooled down to 80 to 150°C, whereby water is condensed out of the gas.